



HOT (Chengdu) Industries Co Ltd

H-TBS Coal Slurry Separator (Hydrosier)

About HOT

HOT (Chengdu) Industries Co Ltd (former HOT Mining) a national high-tech enterprise, is committed to providing the resource industry with services from exploration to pit closure, including consulting and design, core equipment supply, intelligence, and "one-stop" engineering technical service.

HOT has successfully applied the latest technology to mining and mineral processing practice, such as XRT Intelligent Ore Sorter, X-ray Coal Ash & Moisture Analyzer, XRF Pulp Grade Analyzer, Dynamic Density Control for Dense Medium Process, Intelligent Grinding Efficiency Optimization System and other mineral processing intelligent equipment and intelligent process control system.



ABOUT Our Services

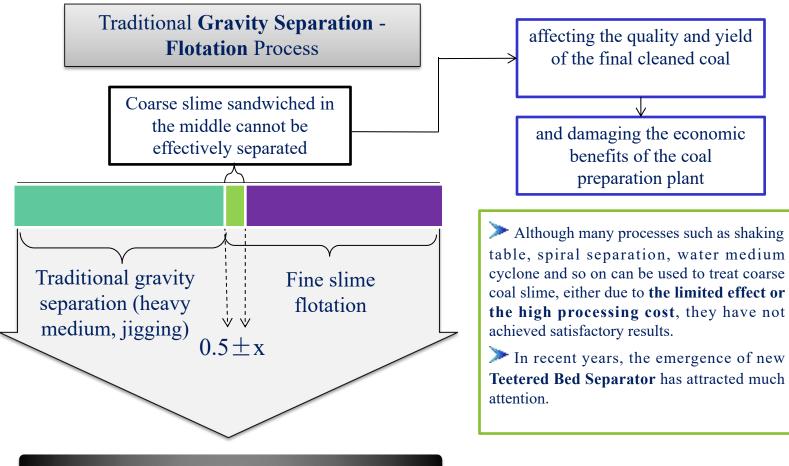
1. Pre-Feasibility Study, Feasibility Study, Concept Design, Engineering Design, Project Budget for Coal Preparation Projects;

- 2. Equipments and Spare Parts——Fans, Cyclone, Centrifuge, Filter Press, spiral, kinds of crushers, TBS,etc;
- **3. Operations for CHPP;**
- 4. Intelligent System for Mining and Coal Washery;
- 5. Materials Handling System & Express Train/Truck Loadout System.



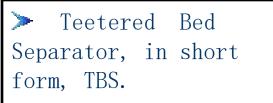
TBS Coal Slurry Separator



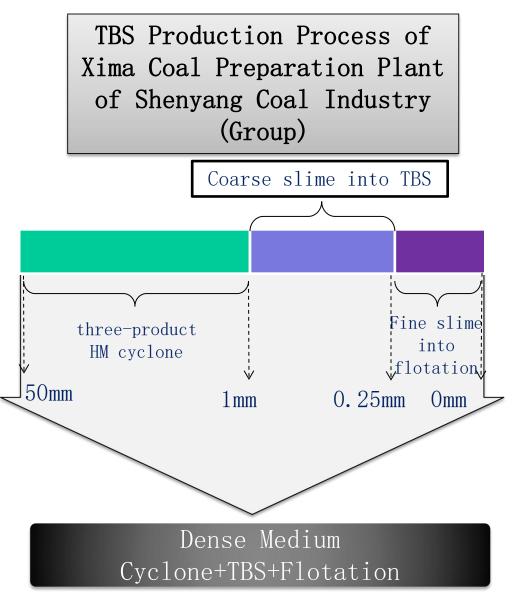


Dense Medium Separation+Flotation





> The first TBS made in the United States was introduced into China and put into operation in September 2005 at Xima Coal Preparation Plant of Shenyang Coal Industry (Group).





Introduction - TBS Advantages and Problems of Imported TBS

TBS Advantages:

Wide sorting granularity (3-0.15mm)

Adjustable separation density $(1.3-1.8g/cm^3)$

No need to add heavy agents and chemicals.

Problems of Imported TBS:

Inadequate pertinence to the nature of incoming materials.

Equipmnet price is too high.

Technical and after-sales services are not timely.

Long parts supply cycle (generally 6 to 8 weeks).

Introduction—HOT H-TBS Series HOT Teetered Bed Separator Prototype





Working Principle: The interference bed separator is a kind of interference sedimentation separation equipment that **uses the rising water flow to generate turbulence** in the cylindrical tank. Due to the different density and particle size of feed particles, the settling speed of particles is different.

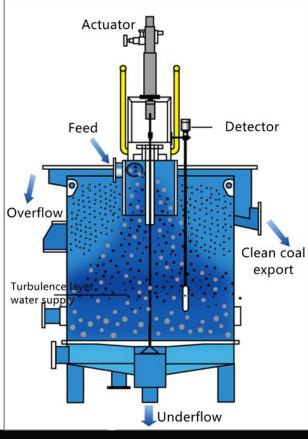


Figure 2-1 Working principle of interference bed separator The role of rising water flow provides conditions

for particle separation:

> When the falling speed of feed particles is equal to the rising water flow speed, he particles are suspended in the separation equipment forming a separation bed;

> When the feed particle speed is less than the rising water flow speed, the particles are carried to the overflow under the action of the rising water flow and become concentrate;

>When the feed particle velocity is greater than the rising water velocity, the particles move downward, pass through the separation bed, become tailings, and discharge from the underflow port, thus realizing the effective separation of concentrate and tailings.

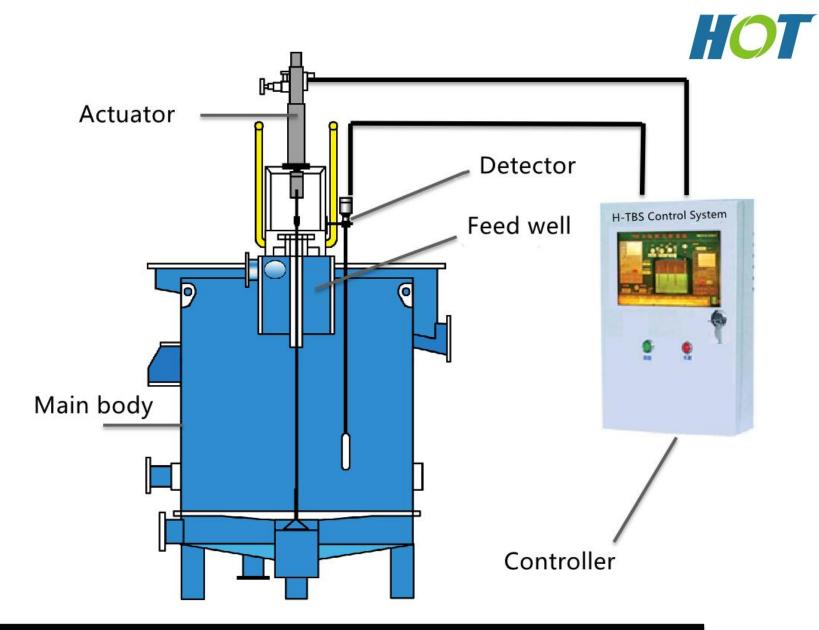
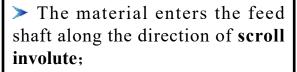


Figure 2-2 Schematic diagram of H-TBS Series Teetered Bed Separator





> The feed well evenly feeds the feed into the interference bed separator, and the feed well is lined with wear-resistant corundum (composition AL2O3) to increase the service life.

> Detector, also known as sensor, is located in the middle of the sorting bed. The density of the turbulent bed in the interference bed separator is different, and the pressure is also different.

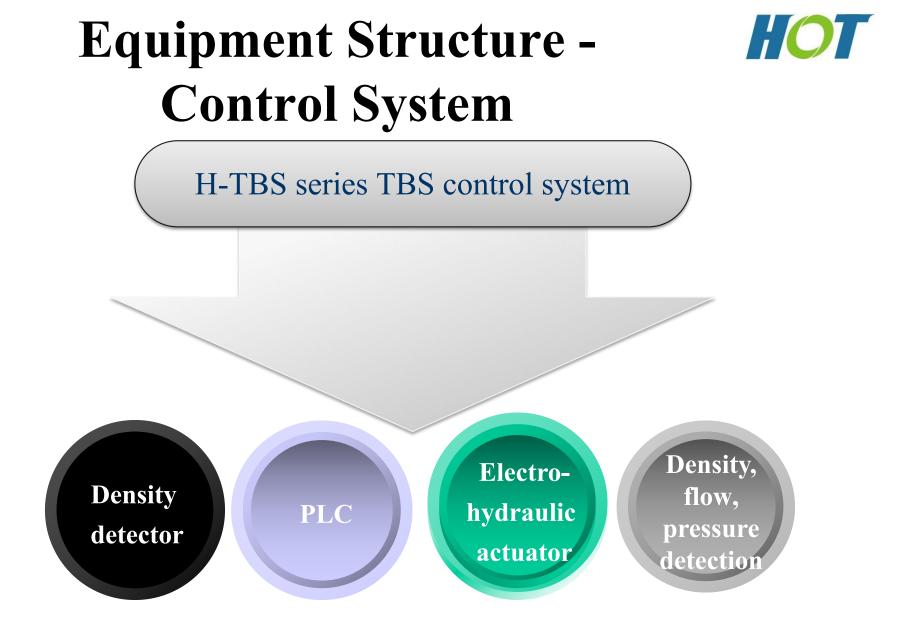
> The H-TBS series interference bed sorter uses the density detector produced by Germany Endershaus Company.

Mainbody The actuator is composed of actuator, connecting rod device, shuttle valve and valve seat. The core of the

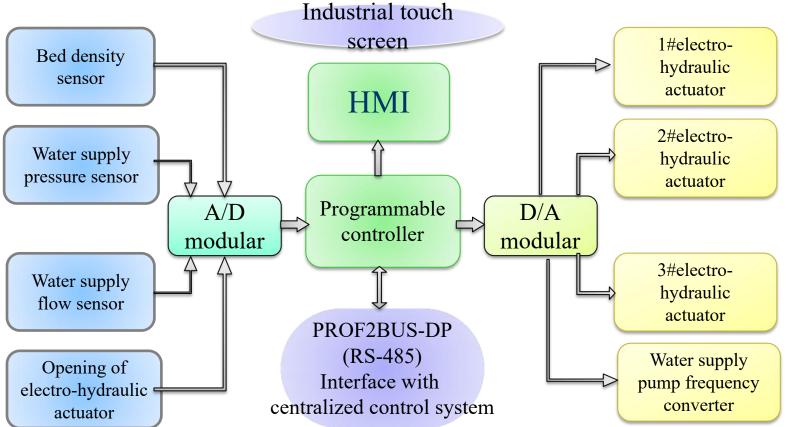
> H - T B S series interference bed sorter uses electro-hydraulic actuator.

actuator is the actuator.

Figure 2-2 Equipment structure composition of H-TBS series TBS



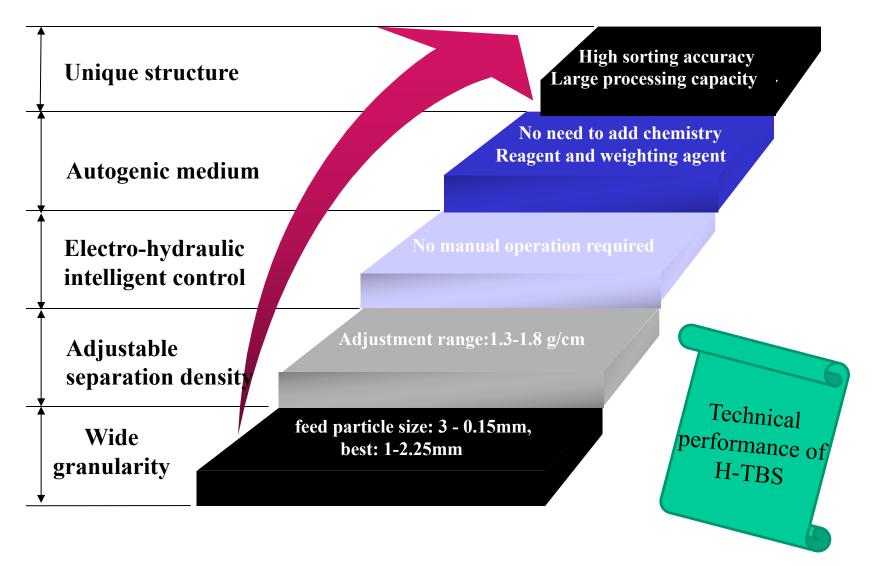
Equipment Structure - Control System



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Figure 2-3 PLC control system block diagram of H-TBS series TBS

2.3 Technical characteristics and performance of H

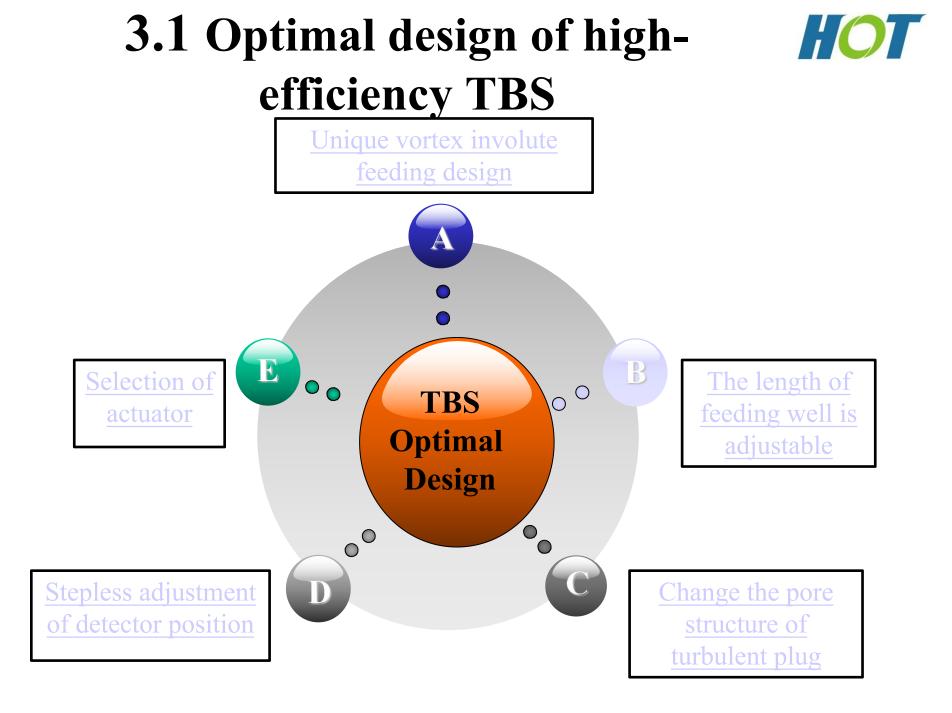


Technical Parameters of H-TBS

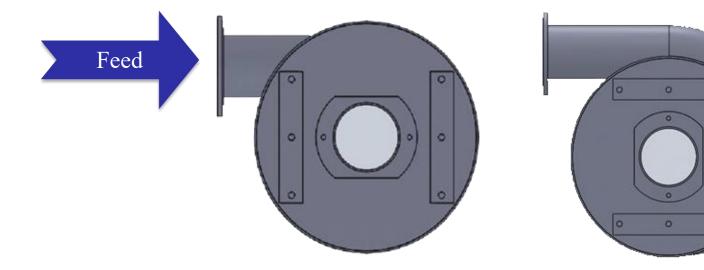
 Table 2-1
 Technical Parameters of H-TBS

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Model Diameter	H-TBS- 1800	H-TBS- 2100	H-TBS- 2400	H-TBS- 3000	H-TBS- 3600
Box diameter(mm)	1800	2100	2400	3000	3600
Process capacity(t/h)	50-60	70-80	90-100	110-130	140-160
Feed size(mm)	1-0.25	1-0.25	1-0.25	1-0.25	1-0.25
Feed concentration(%)	45-50	45-50	45-50	45-50	45-50
Rising water volume(m ³ /h)	50-60	70-80	80-90	90-100	110-120
Rising water pressure(Kpa)	70	70-100	70-100	70-100	80-110
Bed density(g/cm ³)	1.3-1.8	1.3-1.8	1.3-1.8	1.3-1.8	1.3-1.8
Actuator type	Electrohy draulic	Electrohy draulic	Electrohy draulic	Electrohy draulic	Electrohy draulic
Number of tailings discharge outlets	1	1	3	3	4
Actuator power(Kw)	0.55 imes 1	0.55×1	0.55×3	0.55×3	0.55×4







Top view of feed shaft in tangent direction

Top view of vortex involute feed shaft

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Fig. 3-1 Involute Feed Shaft



Compared with the tangent method, the scroll involute feeding method has the following advantages:



A. Optimized design - adjustable length of feed well

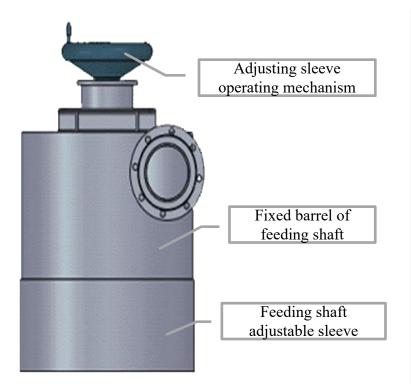


Figure 3-2 Schematic diagram of feeding shaft length adjustable mechanism

The length of the feed well directly affects the separation time and separation effect of the material. The length of feeding pipe set for this test is: > $L_1 = 140$ mm; > $L_2=270$ mm; > $L_3 = 500 \text{mm};$ $> L_4 = 600 \text{mm};$ • When the feed concentration C=300g/L and the water volume Q=81mL/S remain unchanged, See Table 3-1 for the relationship between the length of feed pipe and product quality and sorting effect:

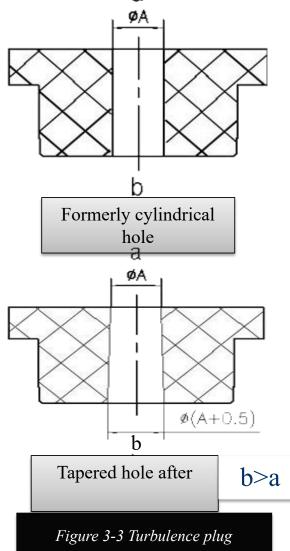
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B. Optimized design - adjustable length of **HOT** feed well

	Table 3-1 Comparison of feeding tube length andsorting effect					
Length ((mm)	Ash content (%)	Quantity efficiency (%)	Imperfectio n (I)	Possible deviation (Ep)	
140)	15.12	95.26	0.133	0.076	
270		12.80	91.31	0.151	0.072	
		12.37	90.18	0.186	0.081	
		1.80	89.65	0.192	0.084	
		From the e	From the experimental results, it can be seen that under the			

condition that some process adjustment factors remain unchanged, the effect of feed pipe length on the separation effect is quite obvious.

C. Optimal design - change the pore structure of the turbulent plug



> In order to solve the problem of turbulence plug plugging, the vertical hole of turbulence plug is changed into a conical hole.

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> In normal production, the rising water flows from b to a, a<b, and the material particles at the end of a are easily impacted by the rising water, and then participate in the separation.

>After stopping, the materials in the interference bed will gather at the top of the turbulence plug under the action of gravity;

> Due to the small hole diameter at the top of the turbulent plug and the large hole diameter at the bottom, even if the material enters the turbulent plug hole, the rising water can easily lift the material in the trapezoidal hole and maintain a good penetration rate.

D. Optimal design - infinite adjustment of detector position

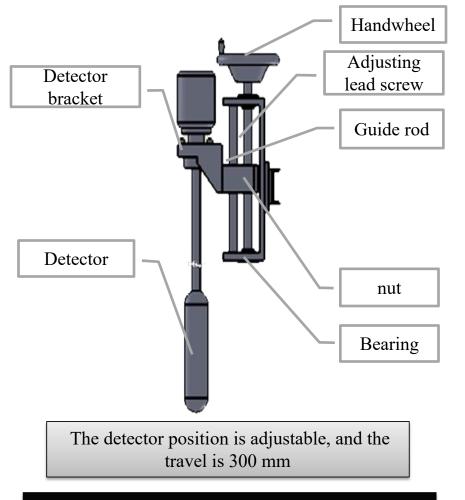


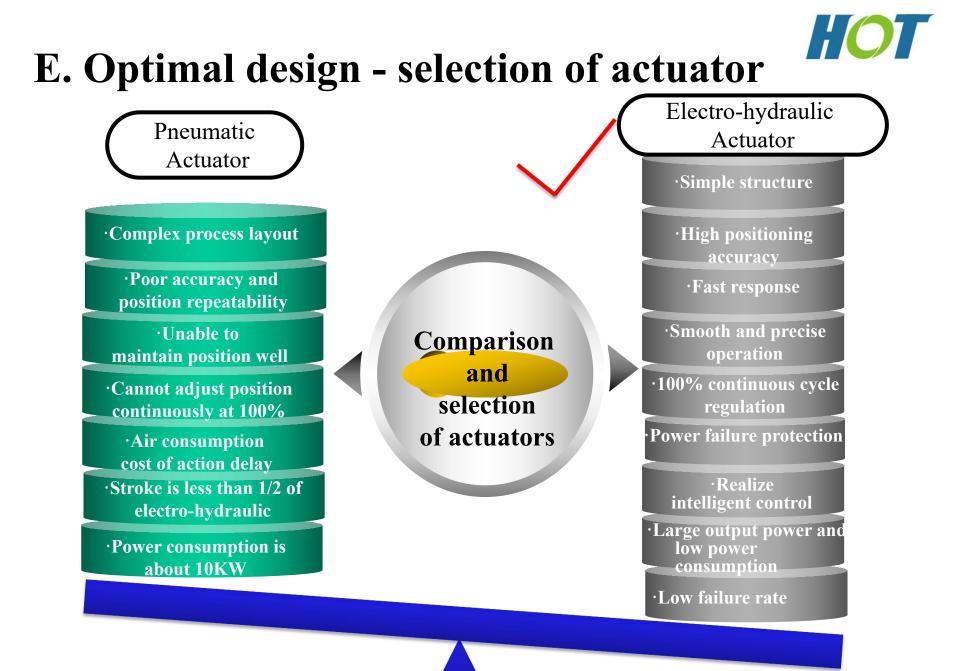
Fig. 3-4 Detector adjustable mechanism

> The position of the separation bed of the interference bed sorter is determined by a variety of factors. Placing the detector at the position that best represents the separation density of the bed can also transmit accurate signals to the actuator.

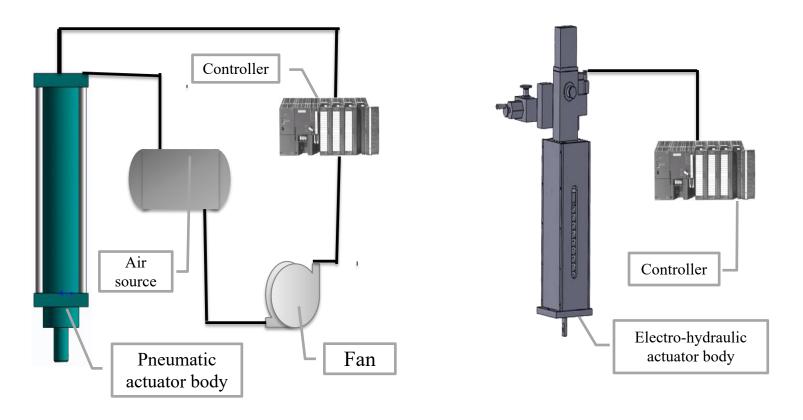
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> See Fig. 6 Detector adjustable mechanism:

> During commissioning, the detector is placed in the middle of the interference bed sorter. In actual operation, the detector is gradually adjusted to the best position according to various indicators and then locked.







Complex pneumatic actuator layout process

Simple electro-hydraulicactuator layout process

Figure 3-5 Schematic diagram for comparison of process layout of pneumatic and electro-hydraulic actuators

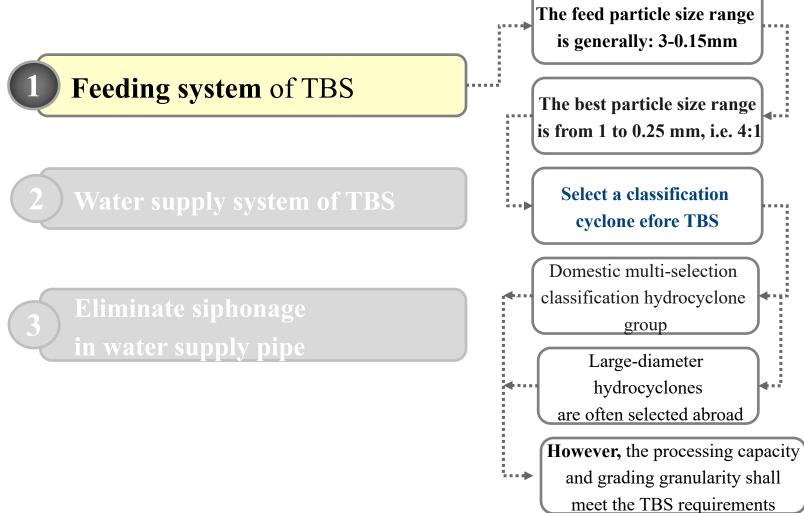


3.2 Optimal design of H-TBS series process system

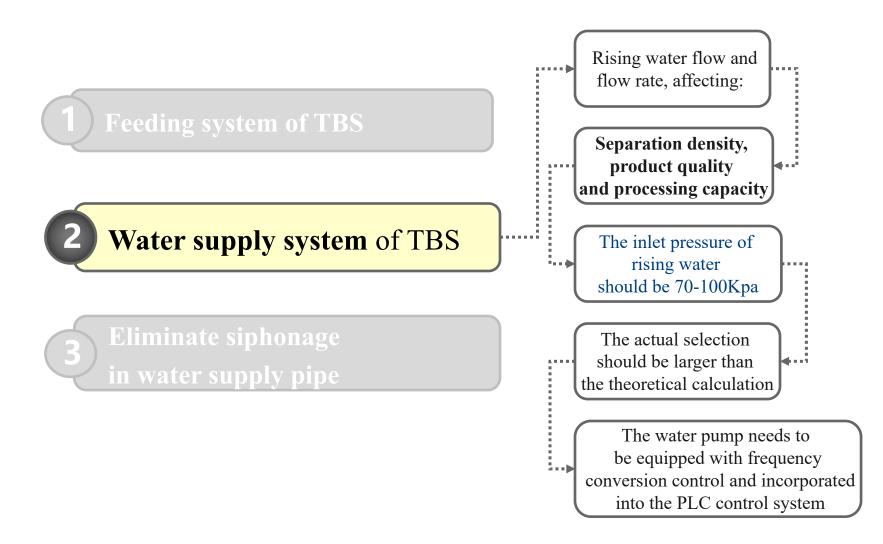
Optimization design of process system				
Feeding system of TBS	Water supply system of TBS	Eliminate siphonage in water supply pipe		



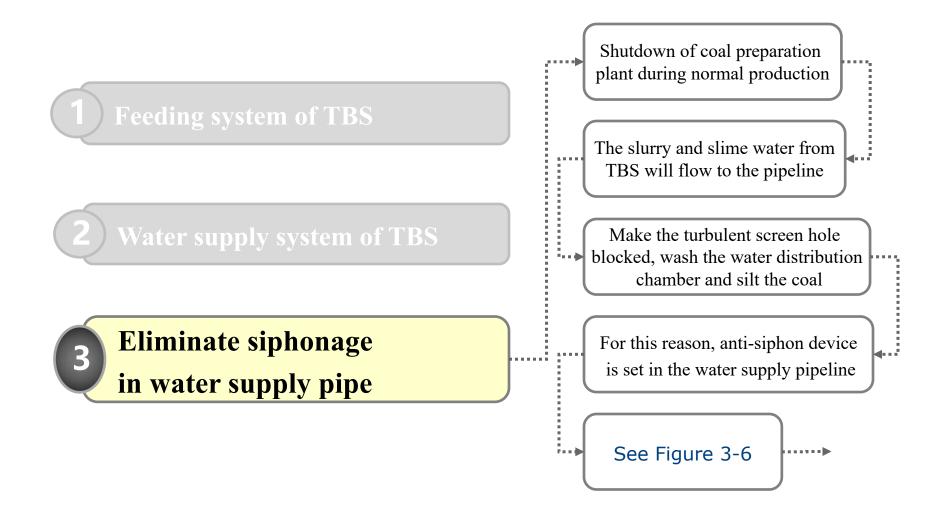














Eliminate siphonage in water supply pipe

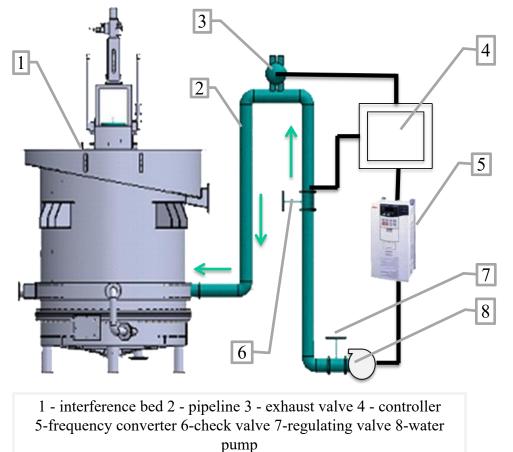
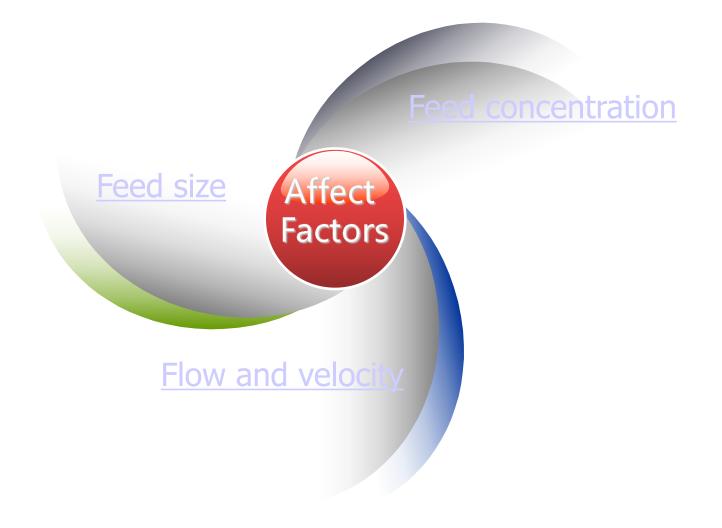


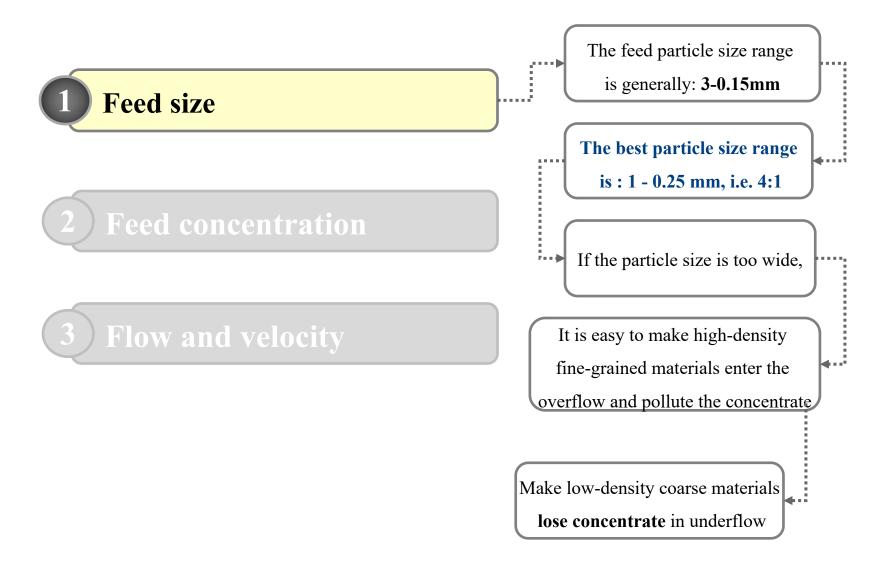
Figure 3-6 Anti-siphon Structure

> After the water pump is shut down, the water stop valve is closed and the exhaust valve is opened at the same time, which interferes with the fact that the slurry in the bed tank is at the same atmospheric pressure as the slime water in the pipeline, and the siphonage phenomenon in the pipeline is eliminated, and the opportunity for the turbulence plug hole to be blocked and the rising water distribution chamber to accumulate slime is significantly reduced.

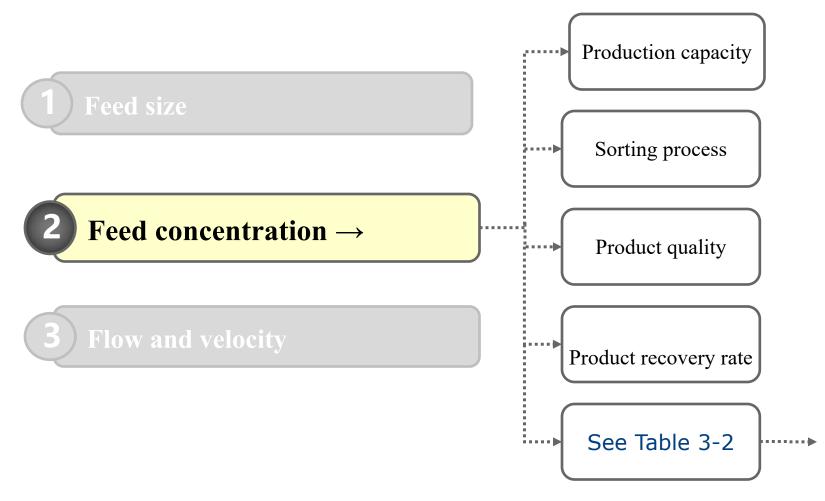




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Feed Concentration

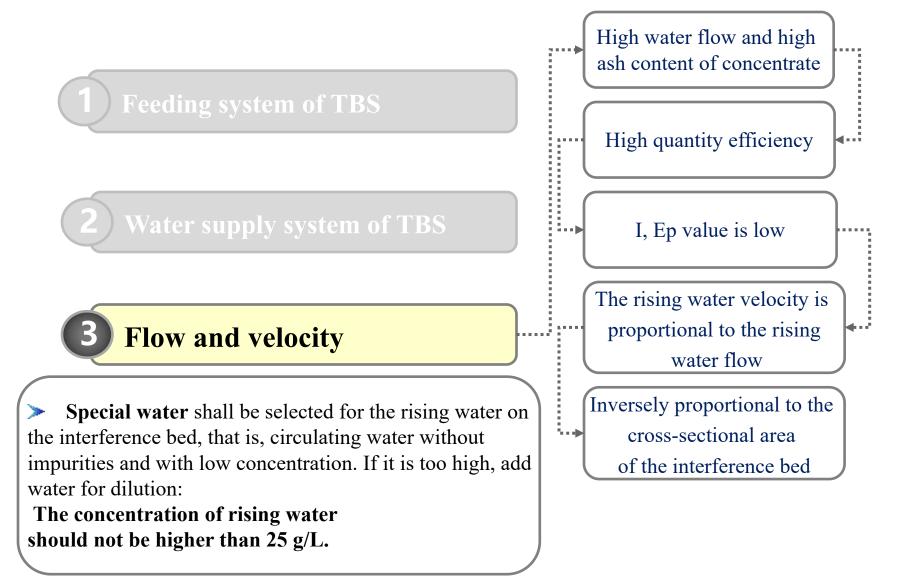
>When the **depth of the feed pipe and the flow rate are constant**, the effect of the feed concentration on the effect of the interference bed.

Table 3-2 Effect of Different Feed Concentrations on the SeparationEffect of Interference Bed Separator

Feed Concentration (g/cm ³)	Product ash (%)	Quantity efficiency (%)	Imperfection (I)	Possible deviation (Ep)
200	12.18	83.58	0.192	0.084
300	12.06	82.24	0.262	0.081
400	11.97	81.91	0.186	0.077
400	11.7/	01.71	0.100	U.U / /
500	12.31	82.40	0.241	0.087

> It can be seen that when the feed concentration is **400 g/cm3**, the ash content, I value and Ep value of the product are the lowest.

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4 Application Cases

The H-TBS-3000 TBS developed by HOT (Chengdu) Industries Co Ltd. was put into use in the dense medium workshop of Hongyang No. 3 Coal Preparation Plant (new plant) of Shenyang Coal Industry (Group) in June 2008.





Hongyang coal preparation plant of No. 3 Coal Mine is a coking coal preparation plant with a design capacity of **5.0Mt/a**, in which the design capacity of the new plant is 2.2Mt/a, and the design capacity of the old plant is 2.8Mt/a. The selected coal is lean coal, with a slime content of more than 35%. 1-2.25mm coarse coal slurry is divided into **32.35%**



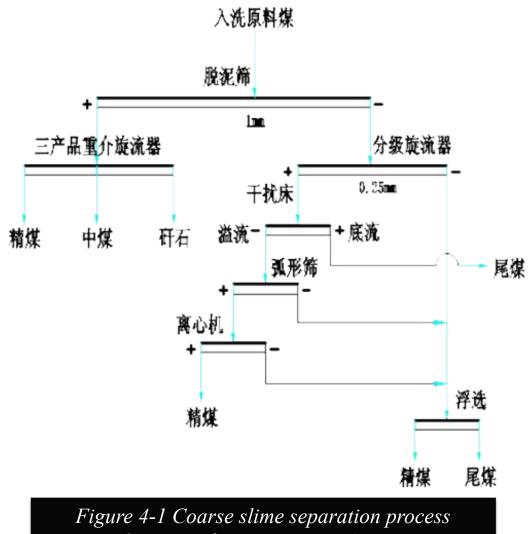


diagram of Hongyang No. 3 Mine

> The coal preparation plant of Hongyang No. 3 Mine adopts a new coal preparation process of d e n s e m e d i u m cyclone+teetered bed separator+flotation.

>See Figure 4-1 for details:

> The main products are Grade 8 and Grade 10 refined coal for smelting, which is used as coking refined coal for Angang Steel and Benxi Steel, and middling coal for nearby power plants or civil use.

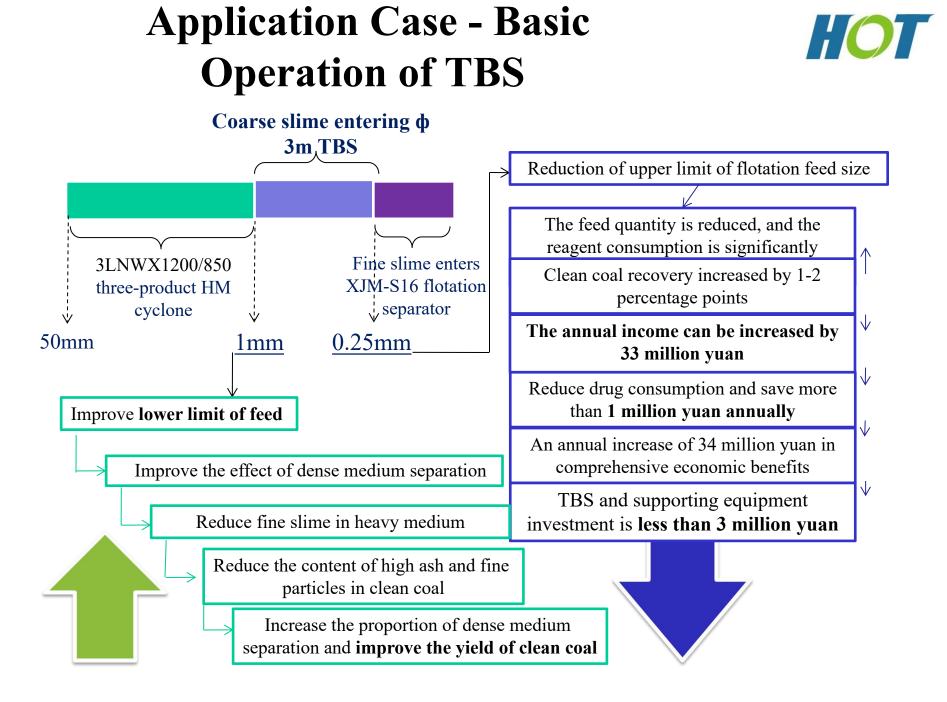
Application Case - Basic Operation of TBS



The production practice for more than one year hows that using XGR-3000 interference bed separator o separate the coarse slime of 1-2.25mm can not only eparate the qualified eight-class clean coal products, but ilso reach 62.40% of tailings ash, and the quantity ifficiency is more than 90%.

Table 4-1 Process parameters of interference bedseparation bed in Hongyang No. 3 Mine

TBS Specificatio (mm)	on Feed Size (mm)	Feed Concentration (%)	Sorting Density (g/cm ³⁾	Rising Water Volume (m ³ /h)	Water Gage (Kpa)	Imper -fection (Ep)	Possible Deviation (I)
φ3000	1-0.25	50	1.49	80	70	0.0625	0.127



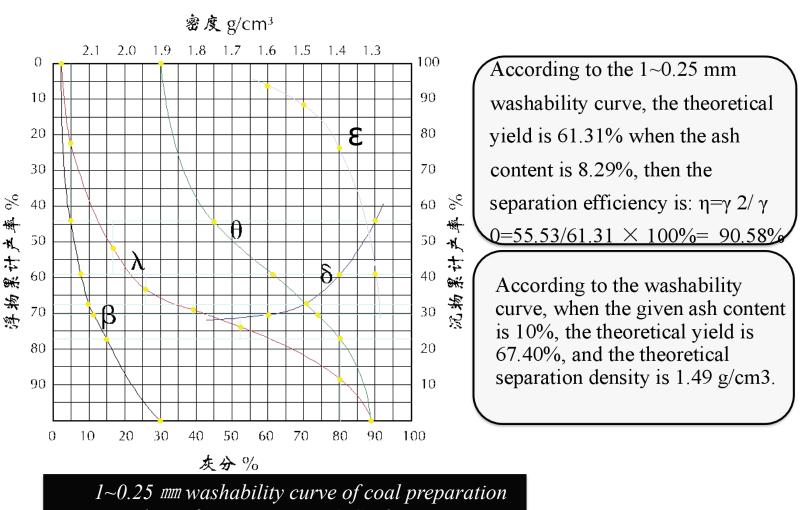
Application Cases -Application Effect of TBS

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Table 4-2 1-2.25mm flotation and sedimentation test of
Hongyang No.3 Coal Preparation Plant

Density level (g/cm ³)	Average density (g/cm ³)	Clean coal			Tail coal			
		Producti vity (%)	Incoming materials (%)	Ash content (%)	producti vity (%)	Incoming materials (%)	Ash content (%)	Allocation rate (%)
1	2	3	4	5	6	7	8	9
<1.3	1.25	74.88	41.85	3.81	0.08	0.03	4.91	0.07
1.3~1.4	1.35	15.32	8.51	14.58	0.14	0.06	14.70	0.7
1.4~1.5	1.45	6.17	3.43	24.27	2.33	1.04	26.53	23.26
1.5~1.6	1.55	2.43	1.34	37.88	7.17	3.18	34.94	70.35
1.6~1.8	1.7	1.21	0.67	65.10	20.45	9.09	47.75	93.13
>1.8	2.1	0	0	0	69.83	29.29	70.88	100
Tptal		100	55.33	8.29	100	44.47	62.40	





plant of Hongyang No. 3 Coal Mine



Advanced TBS

technical indicators:

(Ep=0.0625

I=0.127

η=90.58%)

When the ash

content of raw ore

is 32.35%, **the**

product quality

index is qualified::

(Ash content of concentrate: 8.29%;

Tailings ash content: 62.40%)

Reasonable process parameters:

(separation density 1.493 g/cm3;

Rising water volume 80-100m3/h;

Water inlet pressure 70-80Kpa) H-TBS has achieved obvious results in separating coarse slime (1-2.25mm) from Hongyang No. 3 Mine.







4 Application Cases

Five sets H-TBS-3000 TBS developed by HOT (Chengdu) Industries Co Ltd. was put into use in the dense medium workshop of Ukhaa Khudag (UHG) Coking Coal Washing Plant, Mongolian Mining Corporation during 2007-2020.





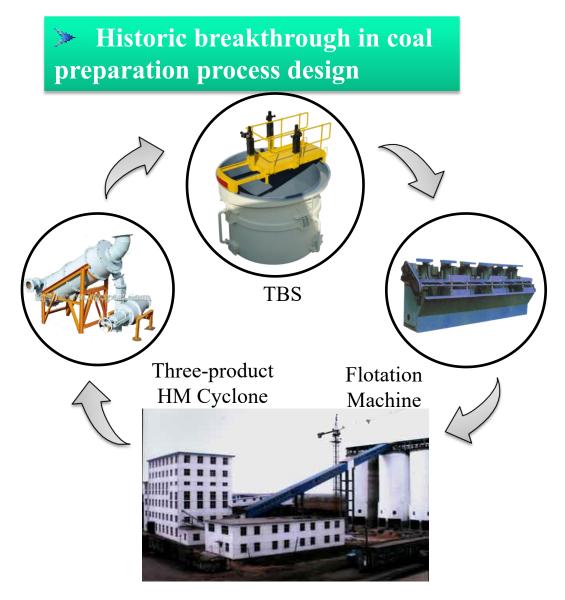
Mongolia UHG coal preparation plant has a total processing capacity of <u>15 Mt/a</u> and is divided into three modules, each of which is 5 million tons. The selected coal is high-quality coking coal. The HTBS-3.0 coarse slime interference bed separator has a separation granularity of <u>2-0.3mm</u> and separation efficiency of <u>>94%</u>.







5 Application Prospect



In 2005, Handan Design Institute independently adopted the combined process of three-product dense medium cyclone+TBS+flot ation for the first time in China, which was successfully used in Xuzhou Zhangshuanglou **Coal Preparation** Plant!



5 Application Prospect

> Ideal equipment for coarse slime separation

Coarse slime separation has always been a difficult problem that the coal preparation industry pays close attention to and is committed to solving. The application of TBS in the coal preparation process makes people see the ideal coarse slime separation equipment.

> Although there are also slime dense medium cyclone and spiral separator to separate coarse slime, the TBS still has obvious

advantages in comprehensive comparison.

5 Application Prospect



> It is matched with spiral separator to improve quality and reduce ash

The minimum separation density of the **TBS** can reach 1.3 g/cm3. If the light products of the spiral separator are washed again with the interference bed separator, high-quality clean coal products can be obtained.







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